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Rapid Production of High-Titer D-Mannitol and Gluconate Catalyzed by a Combination of Whole-Cell and an Enzyme at High Temperatures

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ABSTRACT: D-Mannitol and D-gluconate are value-added biobased chemicals with diverse applications in food, medical, and chemical industries. D-Mannitol can be hydrogenated from hexoses (e.g., D-fructose) catalyzed by microbial fermentation, whole-cell biocatalysis, and purified-enzyme cascade biocatalysis. Here we designed a cell–enzyme system comprised of the whole cells co-expressing both hyperthermophilic mannitol dehydrogenase (MDH) and glucose dehydrogenase (GDH) as well as a hyperthermophilic xylose isomerase (XI). The whole cells have its inherent NAD enabled to implement NAD-self sufficient coupled redox reactions without externally-added NAD and aeration. Four cases of whole cells co-expressed MDH and GDH in *E. coli* BL21(DE3) were compared and optimized by expressing two genes separately or in tandem and changing gene alignment. Also, two-step biotransformation was developed to convert 300 g/L glucose to 129 g/L mannitol and 161 g/L gluconate in a pH-controlled bioreactor at 70 °C. This cell–enzyme system had a high volumetric productivity (10.7 g/L/h mannitol and 13.4 g/L/h gluconate) and a high product yield (91.7%). This study implied that using hyperthermophilic enzymes and cell–enzyme system could open great opportunities for industrial biomanufacturing.

Keywords: D-Mannitol; Gluconate; Whole cell catalysis; Thermophilic enzyme; NAD self-sufficient



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1. Introduction

D-Mannitol (hereafter denoted as mannitol) is a natural six-carbon sugar alcohol widely used in the food, pharmaceutical, and chemical industries [1]. The demand for mannitol as a low-calorie sweetener is steadily increasing in response to the rising global prevalence of obesity and diabetes [2] because it is a non-metabolizable sugar alcohol with about half the sweetness of sucrose [3]. In the pharmaceutical industry, stable and sweet mannitol is used to mask the off-flavors of drugs as a pharmaceutical formulation [4]. It is also used as a dehydrating agent and diuretic [5]. The global market for mannitol was estimated at $451 million in 2024 [6].

Mannitol can be produced by various approaches, including extraction from plants [7], chemical synthesis [8], and bioproduction [9]. Due to modest reaction conditions and high selectivity, mannitol bioproduction from D-fructose is of great interest (Table 1). Bioproduction can be classified by its biocatalysts, from (cascade) enzymes, whole cells, to microbial cells. Cells used for microbial fermentation included yeasts, filamentous fungi [10], and lactic acid bacteria [11,12]. However, fermentative by-products and long fermentation time (typically exceeding 24 h) hindered its wide industrial biomanufacturing. Alternatively, mannitol can be produced from D-fructose via the hydrogenation catalyzed by mannitol dehydrogenase (MDH) with NADH (Figure 1a,b), which can be regenerated from formate catalyzed by formate dehydrogenase (FDH) [3,13,14]. However, this enzymatic conversion suffers from the addition of costly NAD and the use of costly purified enzymes. To address the above weaknesses of the two-enzyme cocktail, the whole-cell

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biocatalysts that contained two redox enzymes have been developed, where the coenzyme NAD was recycled between two enzymes, and NADH can be generated from another substrate formate [15–17] or D-glucose [18].

Biomanufacturing catalyzed by cell–enzyme tandem systems [19] received less attention in the literature. Kaup et al. proposed a recombinant *E. coli* strain co-expressing MDH and FDH to produce mannitol from glucose and an enzyme glucose isomerase (GI) [20]. Mannitol titer reached 150 g/L after 40 h with a productivity of 4.55 g/L/h at 37 °C. However, this method was based on using mesophilic enzymes; the instability and low activity of mesophilic FDH, and other *E. coli* enzymes limited its large-scale application.

In this study, we developed a cell–enzyme system consisted of an *E. coli* strain co-expressing hyperthermophilic MDH (EC 1.1.1.67) from *Thermotoga maritima* and glucose dehydrogenase (GDH, EC 1.1.1.47) from *Sulfolobus solfataricus* as well as the hyperthermophilic enzyme xylose isomerase (XI, EC 5.3.1.5) from *Thermus thermophilus*, which can coproduce high titers of mannitol and gluconate from D-glucose (Figure 1c). Notably, this biotransformation was operated at high temperatures without externally-added NAD. This biotransformation could be a promising method for the industrial co-production of mannitol and gluconate.

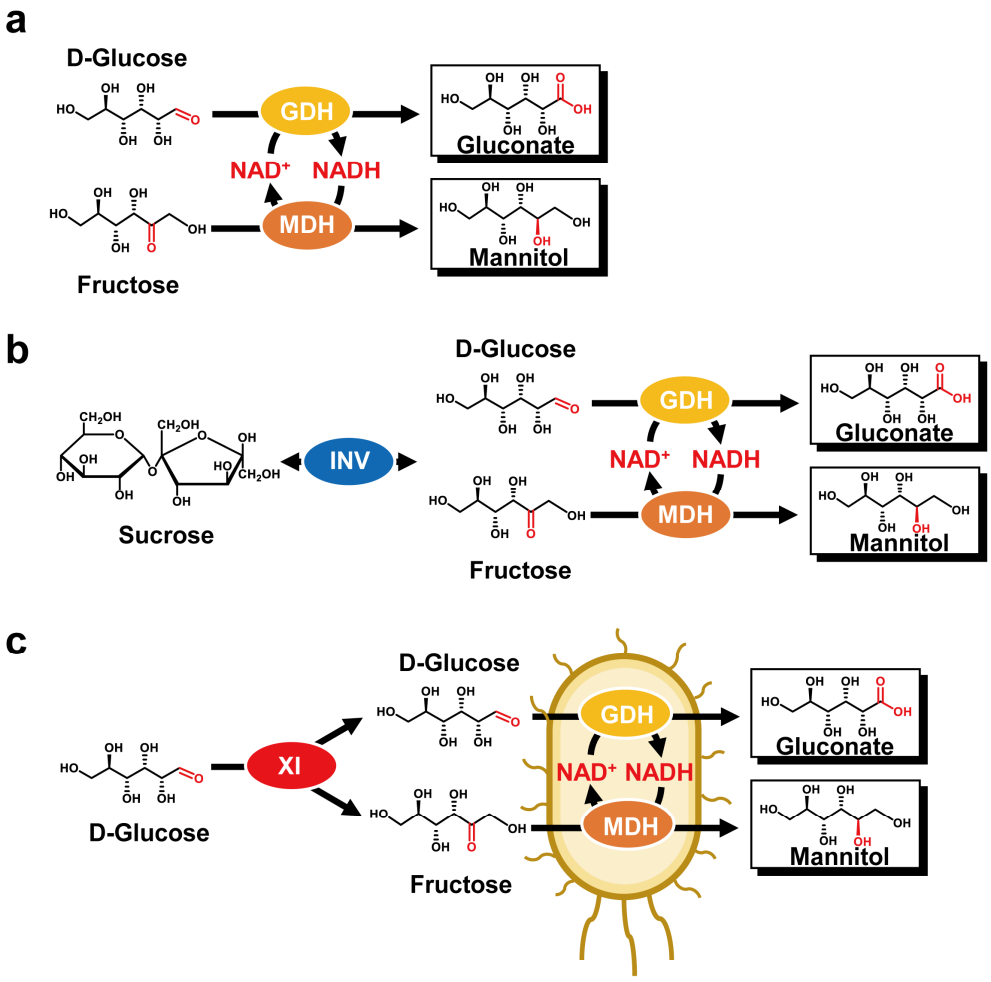


Figure 1. Schematic presentation of the co-production of mannitol and gluconate. (**a**) Two-enzyme biocatalysis based on GDH and MDH. (**b**) Three-enzyme biocatalysis based on GDH, MDH, and invertase (INV). (**c**) Consolidated biocatalysis based on the whole cell expressing GDH, MDH, and XI.

Table 1. Biotransformation strategies used for the production of D-mannitol.

Biocatalytic System	Strategy	Substrates	Temperature (°C)	Time (h)	Titer (g/L)	Productivity (g/(L·h))	Yield (%)	References
Lactobacillus fermentum CRL 573	Fermentation	Glucose, Fructose	37	24	56.8	2.40	94.5	[21]
Candida parapsilosis SK26.001	Fermentation	Glucose	30	120	97.1	0.81	34.2	[22]
Penicillium sp. T2-M10	Fermentation	Glucose	28	168	1.26	0.75×10^{-2}	5.25	[23]
MDH, XI	Enzymes	Glucose, NADH	60	5	3.46	21.9	10.7	[24]
MDH, FDH	Enzymes	Fructose, Formate	25	48	72.0	2.25	80.0	[13]
MDH, FDH	Enzymes	Fructose, Formate	70	40	58.3	4.37	80.0	[14]
IA, αGP, PGM, PGI, M1PDH, M1Pase, FDH, 4GT, PPGK	Enzymes	Maltodextrin, NAD^+	-	48	39.0	-	87.0	[3]
MDH, FDH	Whole cell *E. coli*	Fructose, Formate	30	8	65.9	12.3	72.0	[15]
MDH, FDH	Whole cell *B. megaterium*	Fructose, Formate	-	48	39.3	-	43.7	[17]
MDH, FDH	Whole cell *C. glutamicum*	Fructose, Formate	30	24	87.0	3.48	95.0	[16]
MDH, GDH	Whole cell *E. coli*	Fructose, Glucose	30	24	81.9	10	81.0	[18]
MDH, FDH, GI	Whole cell *E. coli,* GI	Glucose, Formate, NAD^+	37	40	150	4.55	82.0	[20]
MDH, GDH, XI	Whole cell *E. coli,* XI	Glucose	70	12	129	10.7	91.7	This work

Notes: IA: Isoamylase; αGP: α-glucan phosphorylase; PGM: Phosphoglucomutase; PGI: Phosphoglucose isomerase; M1PDH: Mannitol-1-phosphate 5-dehyrogenase; M1Pase: Mannitol 1-phosphatase; 4GT: 4-α-glucanotransferase; PPGK: Polyphosphate glucokinase.

2. Materials and Methods

2.1. Chemicals, Strains, and Media

All chemicals were reagent grade or higher purity, purchased from Sigma-Aldrich (St. Louis, MO, USA), Sinopharm (Shanghai, China), or Aladdin (Shanghai, China), unless otherwise noted. PrimeSTAR Max DNA Polymerase from Takara (Tokyo, Japan) was used for the PCR reactions; other enzymes for molecular biology experiments were purchased from New England Biolabs (NEB, Ipswich, MA, USA). *E. coli* Top10 was used for general molecular cloning, and *E. coli* BL21(DE3) was used for recombinant protein expression. *E. coli* strains were cultivated in a Luria-Bertani (LB) medium at 37 °C. Kanamycin (50 μg/mL) or ampicillin (100 μg/mL) were antibiotics in the LB media.

2.2. Plasmid Construction

The plasmids are summarized in Table 2. The sequences of all PCR primers are listed in Table 3. Primers were synthesized by GENEWIZ (Suzhou, China). All of the plasmid sequences were validated by DNA sequencing.

The plasmid pET28a-MDH contained the *mdh* gene (GenBank no. AAD35386.1) that was amplified from the genomic DNA of *Thermotoga maritima* MSB8 by a primer pair of pET28a-MDH-IF and pET28a-MDH-IR. The pET28a vector backbone was amplified with a primer pair of pET28a-MDH-VF and pET28a-MDH-VR. The plasmid pET28a-MDH, based on two DNA fragments, was obtained using Simple Cloning [25].

For Case One, plasmid pET28a.1-GDH-MDH contained an expression cassette containing the genes *gdh* and *mdh*. The two genes have RBS and share one T7 promoter and T7 terminator. The *mdh* gene with its RBS and T7 terminator was amplified from pET28a-MDH with a primer pair of pET28a.1-GDH-MDH-IF and pET28a.1-GDH-MDH-IR fused with the restriction sequence of *Hin*dIII and *Bam*HI. The *gdh* gene with its T7 promoter, RBS, and pET28a vector backbone was amplified from pET28a-GDH with a primer pair of pET28a.1-GDH-MDH-VF and pET28a.1-GDH-MDH-VR fused with the restriction sequence of *Hin*dIII and *Bam*HI. The corresponding restriction enzyme digested two DNA fragments and then ligated them to generate the two-gene co-expression plasmid pET28a.1-GDH-MDH.

For Case Two, plasmid pET28a.R1-MDH-GDH contained an expression cassette containing the genes *mdh* and *gdh*. The two genes have RBS and share one T7 promoter and T7 terminator. The *gdh* gene with its RBS and T7 terminator was amplified from pET28a-GDH with a primer pair of pET28a.R1-MDH-GDH-IF and pET28a.R1-MDH-GDH-IR, fused with the restriction sequence of *Hin*dIII and *Bam*HI. The *mdh* gene with its T7 promoter, RBS, and pET28a vector backbone was amplified from pET28a-MDH with a primer pair of pET28a.R1-MDH-GDH-VF and pET28a.R1-MDH-GDH-VR fused with the restriction sequence of *Hin*dIII and *Bam*HI. The corresponding restriction enzyme digested two DNA fragments and then ligated them to generate the two-gene co-expression plasmid pET28a.R1-MDH-GDH.

For Case Three, plasmid pET28a.2-GDH-MDH contained an expression cassette containing the genes *gdh* and *mdh*. The two genes have their own T7 promoter, RBS, and T7 terminator. The *mdh* gene with its T7 promoter, RBS, and T7 terminator was amplified from pET28a-MDH with a primer pair of pET28a.2-GDH-MDH-IF and pET28a.2-GDH-MDH-IR fused with the restriction sequence of *Hin*dIII and *Bam*HI. The *gdh* gene with its T7 promoter, RBS, T7 terminator, and pET28a vector backbone was amplified from pET28a-GDH with a primer pair of pET28a.2-GDH-MDH-VF and pET28a.2-GDH-MDH-VR fused with the restriction sequence of *Hin*dIII and *Bam*HI. The corresponding restriction enzyme digested two DNA fragments and then ligated them to generate the two-gene co-expression plasmid pET28a.2-GDH-MDH.

For Case Four, plasmid pET28a.R2-MDH-GDH contained an expression cassette containing the genes *mdh* and *gdh*. The two genes have their own T7 promoter, RBS, and T7 terminator. The *gdh* gene with its T7 promoter, RBS, and T7 terminator was amplified from pET28a-GDH with a primer pair of pET28a.R2-MDH-GDH-IF and pET28a.R2-MDH-GDH-IR, fused with the restriction sequence of *Hin*dIII and *Bam*HI. The *mdh* gene with its T7 promoter, RBS, T7 terminator, and pET28a vector backbone was amplified from pET28a-MDH with a primer pair of pET28a.R2-MDH-GDH-VF and pET28a.R2-MDH-GDH-VR fused with the restriction sequence of *Hin*dIII and *Bam*HI. The corresponding restriction enzyme digested two DNA fragments and then ligated them to generate the two-gene co-expression plasmid pET28a.R2-MDH-GDH.

Table 2. Plasmids used in this study.

Plasmids	Characteristics	Reference
pET28a-GDH	Kan^R, an expression cassette containing the GDH protein cloned from *Sulfolobus solfataricus*	[26]
pET28a-MDH	Kan^R, an expression cassette containing the MDH protein cloned from *Thermotoga maritima*	This work
pET20b-XI	Amp^R, an expression cassette containing the XI protein cloned from *Thermus thermophilus*	[27]
pET28a.1-GDH-MDH	Kan^R, the genes of GDH and MDH have their own RBS; the two genes share one T7 promoter and T7 terminator	This work
pET28a.R1-MDH-GDH	Kan^R, the order of GDH and MDH was reversed based on pET28a. 1-GDH-MDH	This work
pET28a.2-GDH-MDH	Kan^R, the genes of GDH and MDH have their own T7 promoter, RBS, and T7 terminator.	This work
pET28a.R2-MDH-GDH	Kan^R, the order of GDH and MDH was reversed based on pET28a. 2-GDH-MDH	This work

Table 3. Primers used in this study.

Primer	Primer Sequence (5′-3′) [a]	Restriction Site
pET28a-MDH-IF	GTTTAACTTTAAGAAGGAGATATACCAT GAAAGTACTTTTGATAGAAAAACCCGG	
pET28a-MDH-IR	GATCTCAGTGGTGGTGGTGGTGGTG AGAAAAAATTCCCTTCATCAATGCC	
pET-28a-MDH-VF	CATTGATGAAGGGAATTTTTTCTCACC ACCACCACCACCACTGAGATCCGGCTG	
pET-28a-MDH-VR	CAACACTCGCAACACCGGGTTTTTCTATCAAAAG TACTTTCATGGTATATCTCCTTCTTAAAGTTAAAC	
pET28a.1-GDH-MDH-IF	CCCAAGCTTAAGAAGGAGATAT ACATATGAAAGTACTTTTGATAG	*Hin*dIII
pET28a.1-GDH-MDH-IR	CGCGGATCCCGGATATAGTTCCTCCTTTCAGC	*Bam*HI
pET28a.1-GDH-MDH-VF	CGCGGATCCATTGGCGAATGGGACGCG	*Bam*HI
pET28a.1-GDH-MDH-VR	CCCAAGCTTGTTAGCAGCCGGATCTCAGTGG	*Hin*dIII
pET28a.R1-MDH-GDH-IF	CCCAAGCTTAAGAAGGAGATATACCATGGGCAG	*Hin*dIII
pET28a.R1-MDH-GDH-IR	CGCGGATCCCGGATATAGTTCCTCCTTTCAGC	*Bam*HI
pET28a.R1-MDH-GDH-VF	CGCGGATCCATTGGCGAATGGGACGCG	*Bam*HI
pET28a.R1-MDH-GDH-VR	CCCAAGCTTGTTAGCAGCCGGATCTCAGTGG	*Hin*dIII
pET28a.2-GDH-MDH-IF	CCCAAGCTTCTCGATCCCGCGAAATTAATACG	*Hin*dIII
pET28a.2-GDH-MDH-IR	CGCGGATCCCGGATATAGTTCCTCCTTTCAGC	*Bam*HI
pET28a.2-GDH-MDH-VF	CGCGGATCCATTGGCGAATGGGACGC	*Bam*HI
pET28a.2-GDH-MDH-VR	CCCAAGCTTCGGATATAGTTCCTCCTTTCAGC	*Hin*dIII
pET28a.R2-MDH-GDH-IF	CCCAAGCTTCTCGATCCCGCGAAATTAATACG	*Hin*dIII
pET28a.R2-MDH-GDH-IR	CGCGGATCCCGGATATAGTTCCTCCTTTCAGC	*Bam*HI
pET28a.R2-MDH-GDH-VF	CGCGGATCCATTGGCGAATGGGACGC	*Bam*HI
pET28a.R2-MDH-GDH-VR	CCCAAGCTTCGGATATAGTTCCTCCTTTCAGC	*Hin*dIII

[a] Notes: The restriction sites are underlined.

2.3. Preparation of Whole Cells and Enzymes

The plasmids were transformed into *E. coli* BL21 (DE3) for enzyme expression. Cells transformed with the plasmid were grown on LB agar plates with the appropriate antibiotic at 37 °C overnight. Colonies were chosen for inoculation in 5 mL of LB medium at 37 °C until the absorbance at 600 nm reached about 0.6–0.8. Then 100 μM isopropyl-β-D-thiogalactopyranoside (IPTG) was added to induce protein expression at 16 °C for 18 h. Fermentation broth was centrifuged at 6000× *g* for 10 min, and the cell pellets were washed twice using 0.9% sodium chloride solution. Recombinant cells containing MDH and GDH were harvested and suspended in 50 mM 4-(2-hydroxyethyl)-1-piperazineethanesulfonic acid (HEPES) buffer (pH 7.0) for further use. The protein expression levels of each recombinant *E. coli* were evaluated using SDS-PAGE after ultrasonication with the MIULAB UC-650 (Hangzhou, China; 2 s pulse, total 600 s, at 70% amplitude). The cell lysate containing XI was treated in a water bath at 70 °C for 30 min after centrifugation. After centrifugation at 12,000× *g* for 5 min, nearly pure XI was obtained in the supernatant.

Protein concentration was measured using the Thermo Scientific Pierce Bradford method with bovine serum albumin as a reference protein.

2.4. Comparison of Biocatalytic Efficiency among Four Whole-Cell Cases

Whole-cell reactions were performed in 3 mL of 200 mM HEPES buffer (pH 7.0) containing 20 mM glucose, 20 mM fructose, and 20 OD whole-cells harboring plasmid cases One to Four at 80 °C. Reaction samples were withdrawn at different times. The reactions were terminated by boiling for 10 min. After centrifugation, supernatants were used to quantify intermediates, substrate, and products.

2.5. One-Step Biotransformation from Glucose

The one-step experiment was conducted in a 100 mL pH-controlled bioreactor with a reaction volume of 40 mL, the reaction medium containing 50 g/L glucose, 0.5 g/L XI, five mM $MnCl_2$, and 25 OD whole cells (Case Four) was performed at 80 °C with stirring at 350 rpm. The pH of the reaction mixture was maintained at pH 7.0 by using 2 M NaOH with a pH controller. Reaction temperatures of 60, 70, 80, and 90 °C were tested to determine the optimal temperature. High substrate concentration of D-glucose (300 g/L) was conducted at 70 °C with a stirring rate of 350 rpm. The cell–enzyme system contained 3 g/L XI, 150 OD whole cells (Case Four) and 5 mM $MnCl_2$.

2.6. Two-Step Biotransformation from Glucose

The first-step biotransformation containing 300 g/L glucose, 3 g/L XI, and 5 mM $MnCl_2$ was conducted at 70 °C. When nearly half of the glucose was converted to fructose, the second-step biotransformation was conducted by adding 150 OD of whole cells (Case Four). The pH of the reaction mixture was maintained at pH 7.0 by using 2 M NaOH with a pH controller.

2.7. Analysis

The concentrations of glucose, fructose, mannitol, and gluconate were determined using HPLC (Shimadzu, Kyoto, Japan) equipped with a Waters Sugar-Pak column (Milford, MA, USA) and a refractive index detector. The column set at 80 °C was eluted at 0.5 $mL \cdot min^{-1}$ with a mobile phase of deionized water. Samples were initially diluted in water, followed by filtration through a 0.22 μm hydrophilic poly-(tetrafluoroethylene) syringe filter (Anpel, Shanghai, China). Finally, ten μL of the sample was applied to the column. The data were analyzed and processed using LabSolutions LCGC software (Shimadzu, Kyoto, Japan).

Yields of mannitol, gluconate, and their lumped yield were calculated as following Equations (1)–(3):

$$Y_{\text{mannitol}}\,(\%) = \frac{\text{moles of mannitol}}{\text{initial moles of glucose}} \times 100 \quad (1)$$

$$Y_{\text{gluconate}}\,(\%) = \frac{\text{moles of gluconate}}{\text{initial moles of glucose}} \times 100 \quad (2)$$

$$Y_{\text{Lumped}}\,(\%) = \frac{\text{moles of mannitol} + \text{moles of gluconate}}{\text{initial moles of glucose}} \times 100 \quad (3)$$

3. Results

3.1. The Design of A Biocatalyst Cocktail

The goal of this study was the production of mannitol from glucose, along with the coproduction of gluconate. MDH (EC 1.1.1.67) can convert D-fructose to mannitol via the hydrogenation from NADH, which can be regenerated from D-glucose catalyzed by GDH (EC 1.1.1.47). To avoid the addition of costly NAD and simplify the purification of MDH and GDH, it was designed that the co-expression of MDH and GDH in one host facilitated the NAD self-sufficient coupled reactions without NAD (Figure 1c). This whole-cell biocatalyst can convert equal amounts of D-fructose and D-glucose to mannitol and gluconate. Furthermore, using XI enabled the interconversion of D-glucose and D-fructose to reach an equilibrium. As a result, the MDH- and GDH-expressed whole-cell and a purified XI can make both mannitol and gluconate from glucose.

Due to the numerous advantages of hyperthermophilic enzymes in industrial biomanufacturing [28–31], we carefully chose MDH from *T. maritima* [24], GDH from *S. solfataricus* [32], and XI from *T. thermophilus* [27] by considering their optimum temperatures, specific activities, and functional expression levels in *E. coli* BL21(DE3).

3.2. Optimization of Four Whole-Cell Systems Co-Expressing MDH and GDH

To precisely control MDH and GDH expression levels to balance redox catalytic steps, we constructed four plasmids co-expressing these two genes in different configurations (Figure 2b). Four cases were compared to investigate the effects of the organization of the T7 promoter, T7 terminator, and two-gene order in one vector. In Case One, the *gdh* and *mdh* genes were assembled as a gene cluster, with the *gdh* gene upstream of *mdh*. In Case Two, the order of the two genes was reversed compared to that of Case One. In Case Three, the *gdh* and *mdh* genes were controlled by their own T7 promoter and T7 terminator, and the *gdh* gene was upstream of the *mdh*. In Case Four, the order of the *gdh* and *mdh* genes was reversed compared to Case Three. As shown in Figure 2c, both GDH and MDH were expressed solubly when they were expressed in *E. coli* individually (Figure 2c, lanes 1–3), and these two enzymes also were co-expressed as soluble proteins in four strains containing Case One (Figure 2c, lanes 4 and 5), Case Two (Figure 2c, lanes 6 and 7), Case Three (Figure 2c, lanes 8 and 9) and Case Four (Figure 2c, lanes 10 and 11), the expression levels of GDH and MDH showed significant different among the four strains.

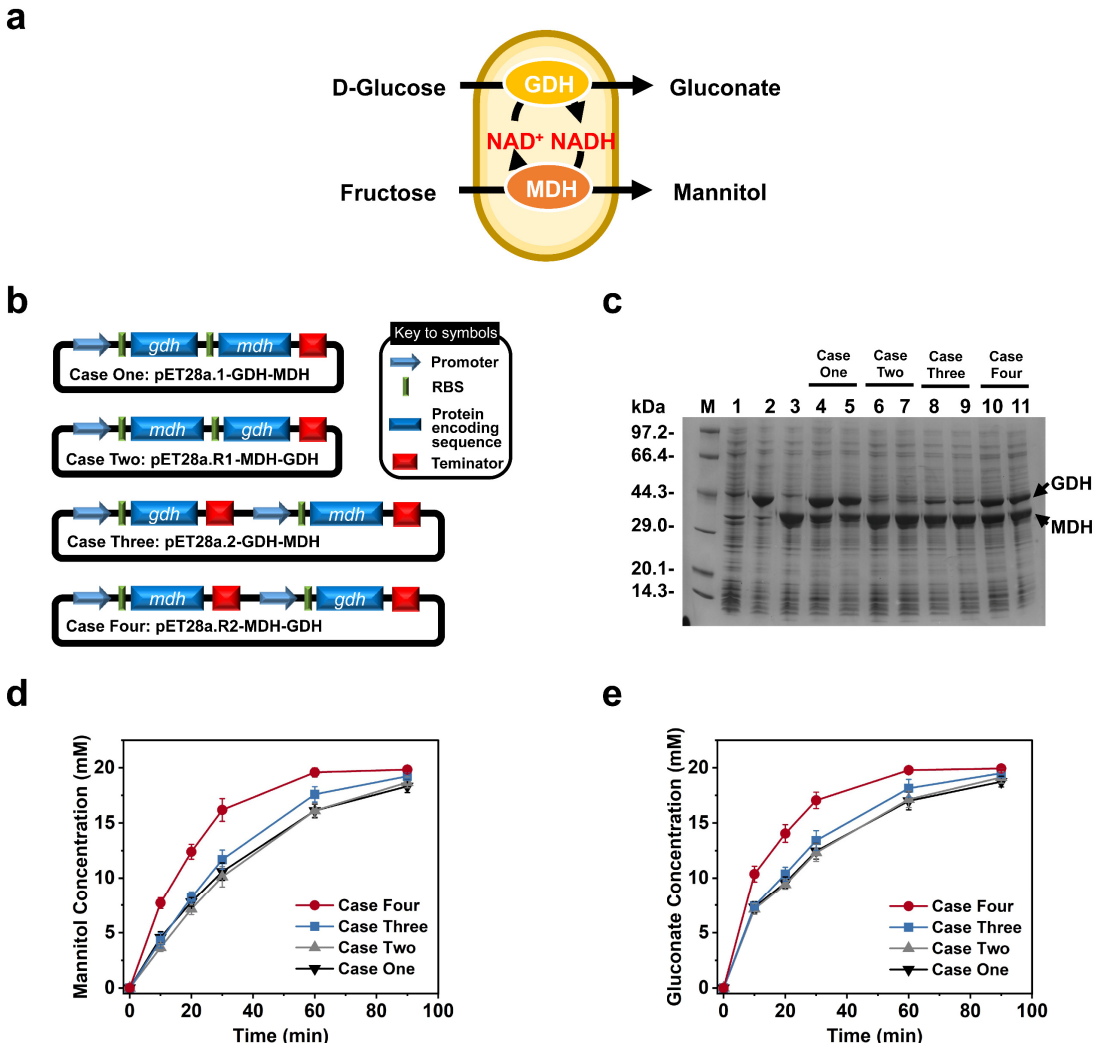


Figure 2. Construction and comparison of four whole-cell systems. (**a**) Schematic representation of the co-production of mannitol and gluconate using a whole-cell biocatalysis system expressing GDH and MDH. (**b**) Plasmid maps of four cases for co-expression of *gdh* and *mdh*: Case One, two genes were assembled as a gene cluster; Case Two, the order of the *gdh* and *mdh* genes was reversed based on Case One; Case Three, each gene was controlled by its own T7 promoter and T7 terminator; Case Four, the order of the *gdh* and *mdh* genes was reversed from Case Three. (**c**) SDS-PAGE analysis of the *E. coli* cell extract of four cases. Lane M, protein marker; Lane 1, total proteins of *E. coli*/pET28a; Lane 2, supernatant of *E. coli*/pET28a-GDH; Lane 3, supernatant of *E. coli*/pET28a-MDH; Lane 4 and 5 are the total proteins and supernatant of Case One, respectively; Lane 6 and 7 are the total proteins

and supernatant of Case Two, respectively; Lane 8 and 9 are the total proteins and supernatant of Case Three, respectively; Lane 10 and 11 are the total proteins and supernatant of Case Four, respectively. The arrows indicate the expressed GDH and MDH in *E. coli*—comparison of the production of (**d**) mannitol and (**e**) gluconate by four co-expression whole cell cases.

In Case One and Case Two, two genes were expressed as a cluster, but the order of the genes was reversed. In Case One, the expression level of GDH was higher than that of MDH, while in Case Two, the opposite was observed. A comparison between Case One and Two suggested that upstream genes typically exhibit higher expression levels than downstream genes. For Case Three and Case Four, each gene was controlled by its own T7 promoter and T7 terminator, making the expression of each gene independent of the other. The expression level of MDH was higher in Case Three than in Case One, and the expression level of GDH was higher in Case Four than in Case Two. Comparisons between Case One and Case Three, as well as Case Two and Case Four, indicated that including a T7 terminator behind each gene helps to enhance the expression of the following gene. These findings suggest that the organization of the T7 promoter, T7 terminator, and the order of genes in a vector may influence the expression levels of the two enzymes. Therefore, the plasmid configuration should be carefully considered when co-expressing enzymes in a single plasmid.

The four whole cell systems co-expressing MDH and GDH were used to convert fructose and glucose into the respective mannitol and gluconate at pH 7.0. The concentrations of mannitol and gluconate increased rapidly during the first thirty minutes, and the reactions leveled off over the next sixty minutes (Figure 2d,e). In all four cases, substrates were converted entirely to products at the end of the reactions. However, when whole cells from Case Four were used as catalysts, the productivities of mannitol (Figure 2d) and gluconate (Figure 2e) were highest, probably owing to the similar expression levels of MDH and GDH in Case Four. Thus, the Case Four strain was chosen to produce mannitol and gluconate for the following experiments.

3.3. Coproduction of Mannitol and Gluconate from Glucose

To coproduce mannitol and gluconate from glucose, we added the purified XI to the whole cell system (Figure 3a). The *E. coli* strain expressed Hyperthermophilic XI, and its cell lysate was heat-treated to obtain a purified XI (Figure S1). The reaction was conducted in a 100-mL bioreactor at 80 °C for 6 h. When 50 g/L glucose was used as substrate, there was a fructose peak at 0.25 h; at this point, 20.0 g/L fructose had been generated. Subsequently, the concentration of fructose decreased in parallel with glucose. Mannitol and gluconate were produced quickly during the first 1 h, followed by a slowing down. At 6 h, the biocatalyst cocktail made 17.0 g/L mannitol and 18.8 g/L gluconate, corresponding to a lumped product yield of 68.1% (Figure 3b). These results showed the feasibility of the cell–enzyme (tandem) system. However, the yield was relatively low, necessitating further optimization.

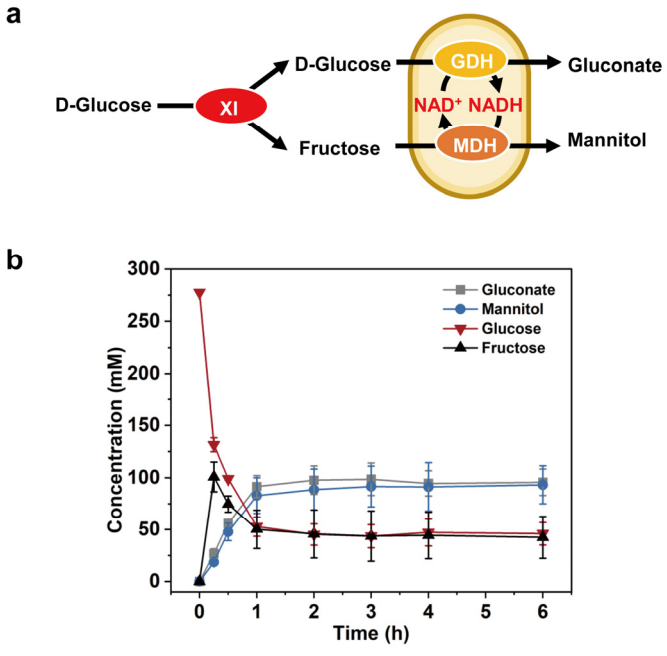


Figure 3. Proof-of-concept experiments for the co-production of mannitol and gluconate from glucose. (**a**) Schematic representation of co-production of mannitol and gluconate from glucose using the whole cell and XI. (**b**) Time profile of co-production of mannitol and gluconate by the whole-cell (Case Four) from 50 g/L glucose at 80 °C. Values shown are means of triplicate determinations.

The reaction temperature was optimized from 60 to 90 °C (Figure 4) because it influenced the specific activities of enzymes, cellular membrane intactness, and substrate/product diffusion. The concentrations of mannitol and gluconate were almost equal at 60–80 °C, while the concentration of gluconate was 14.4% higher than that of mannitol at 90 °C. At 60 °C, the lumped yield was lowest. When the reaction temperature was elevated to 70 °C, two products were mildly increased, probably owing to low enzyme activities at 60 °C for all three enzymes. When the reaction temperature was further increased to 80 and 90 °C, the yields significantly decreased, probably due to the thermal deactivation of enzymes. It was found that the optimal reaction temperature was 70 °C, and the lumped yield was enhanced from 68.1% at 80 °C to 92.0% at 70 °C.

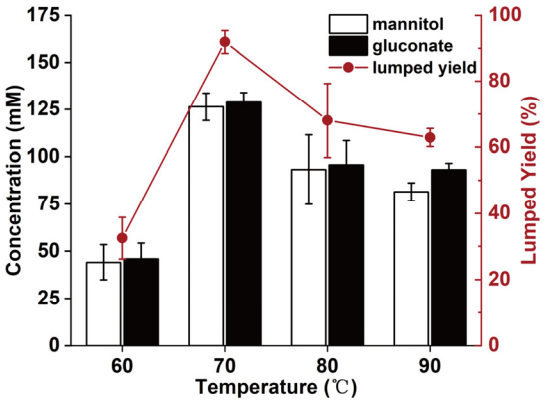


Figure 4. Effects of reaction temperature of *E. coli*/pET28a.R2-MDH-GDH whole cell (Case Four).

3.4. One-Pot Biotransformation in Two Operative Modes

The glucose concentration was increased to 300 g/L, and the enzyme and cell loadings were also increased by six-fold. As the glucose concentration increased, it took longer to reach the steady state. One-step bioprocess that simultaneously added XI and whole cells was proposed (Figure 5a). During the first 2 h of the reaction, the glucose concentration decreased sharply, while the intermediate fructose concentration increased significantly; the concentration of fructose remained consistently much lower than that of glucose. A peak in fructose concentration was observed at 2 h, with 102 g/L of fructose produced. After this point, both glucose and fructose decreased slowly and synchronously. The reaction reached equilibrium around 12 h, yielding 80 g/L of mannitol and 100 g/L of gluconate, corresponding to productivities of 6.67 g/L/h for mannitol and 8.34 g/L/h for gluconate. However, the lumped yield was only 57.0%. The rationale for a switch from a one-step to a two-step process was the kinetic mismatch between MDH on fructose and GDH on glucose. When XI loading was small, the ratio of glucose to fructose was far higher than one, resulting in a mismatch of activities between MDH and GDH. When XI loading was sufficient, resulting in nearly equal molar ratios of glucose to fructose, the matching activities of MDH and GDH led to fast synthesis rates for both MDH and GDH.

A two-step bioprocess was proposed to match the rates of MDH and GDH (Figure 5b). XI was added to transform half of the glucose into fructose at the first step, and then the *E. coli* cells were added to the reactor at the second step. During the first 2 h of the reaction, glucose was sharply isomerized to fructose. 155 g/L Fructose had been produced at 2 h, while the glucose concentration decreased to 141 g/L. With the addition of whole cells, the concentration of mannitol and gluconate in the reaction system quickly increases to 110 and 139 g/L from the consumption of 98 g/L fructose and 134 g/L glucose, respectively, in the first 4 h. The productivity of mannitol was sped up from 6.67 g/L/h to 10.7 g/L/h relative to Figure 5a upon optimization, as equilibrium was reached at 12 h. It was observed that the reaction solution was browning throughout the experiments. At equilibrium, the final mannitol and gluconate concentrations increased to 129 and 161 g/L, respectively, with a lumped yield of 91.7%, significantly higher than the product yield of 57.0% in the one-step experiment.

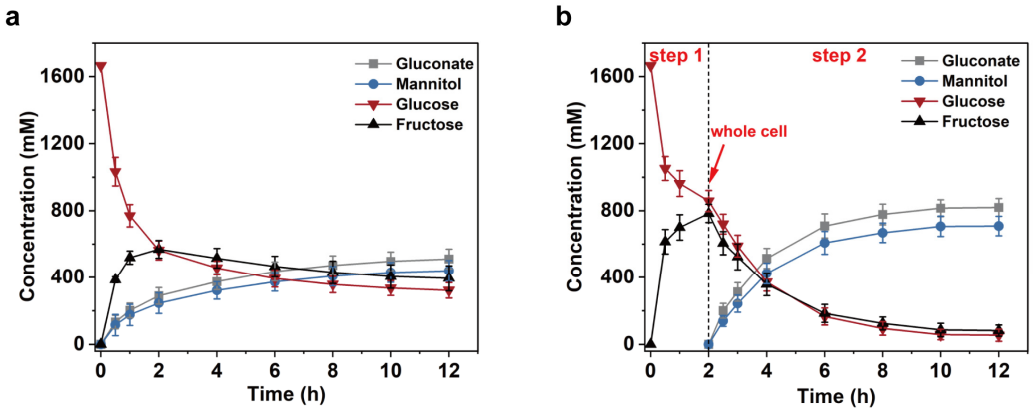


Figure 5. Time profiles of mannitol and gluconate biotransformation from 300 g/L glucose catalyzed by a combined biocatalyst containing the whole cell and XI in two operative modes: (**a**) one-step and (**b**) two-step.

4. Discussion

We combined the whole-cell co-expressing MDH and GDH and a purified XI to coproduce high titers of mannitol and gluconate from glucose at high temperatures. The use of thermostable enzymes XI, GDH, and MDH, the optimization of the two-enzyme expression, the use of NAD internally-regeneration in whole cells, and the employment of the two-step operation mode enabled the production of approximately 129 g/L mannitol and 161 g/L gluconate from 300 g/L glucose. As compared to the previous reports of mannitol production, this method features many advantages: (i) the use of the three hyper-thermophilic enzymes, facilitating high reaction temperature with such features as low viscosity, easy preparation of enzymes [33], deactivation of *E. coli* inherent enzymes [34], low contamination risks; (ii) the use of glucose as a single substrate, rather than a mixed substrate containing both D-fructose and D-glucose; and (iii) high titers, high yields, and productivity (Table 1).

In this study, we employed a combination of whole cell and a purified enzyme. Whole-cell biocatalysts not only avoid the addition of costly NAD, but also the cell membrane enables to two adjacent MDH and GDH to recycle NAD rapidly [35]. Initially, we attempted to co-express three enzymes in one host by constructing the pACYCduet-XI plasmid and co-expressing it with the plasmid co-expressing MDH and GDH in *E. coli* BL21. The low expression level of XI resulted in a very slow initial reaction rate (data not shown). Therefore, we added a purified XI to the whole cells. The loading of XI can be optimized easily to match the enzyme and the whole cells.

The coproduction of gluconate and mannitol could be operative because the latter has a much lower water solubility than gluconate (*i.e.*, 130 g/L for mannitol compared to 620 g/L for gluconate) [36]. After simple crystallization, sodium gluconate in the supernatant could be used directly as a concrete set retarder. The market size of gluconate is far larger than that of mannitol, especially sodium gluconate, which functions primarily as a concrete set retarder, slowing down the initial setting and hardening of the cement paste [37,38].

To further implement the industrial applicability of this biocatalyst cocktail, several issues need to be addressed to decrease biocatalyst costs involving both whole cells and XI. First, coating cells with a protective shell, such as metal−organic frameworks [39], mineralized oxides [29], and polyphenols [40] could be applied to prolong the lifetime of whole cells and restrict more efficiency of NAD self-sufficient recycling. Second, XI could be immobilized [41] or displayed on the surface of whole cells [42] to prolong the lifetime. Third, all of these three enzymes could be engineered for better thermostability and more activity [43,44]. The browning was developing in the scaled-up reaction with high substrate concentrations, possibly due to the Maillard reaction. The reducing sugar reacts with the amino acid groups of enzymes in the Maillard reaction, impairing enzyme activity [45,46]. To minimize the potential impact of the Maillard reaction, it could be controlled by lowering the pH [47], reducing the temperature [48], and decreasing the oxygen levels [45].

In conclusion, we demonstrated that mannitol and gluconate can be produced from glucose in a pH-controlled bioreactor using a cell–enzyme tandem system at 70 °C. This biotransformation that did not need the addition of NAD produced approximately 129 g/L mannitol and 161 g/L gluconate from 300 g/L glucose. It had high product titers, yields, and productivity (Table 1). The use of hyperthermophilic enzymes, regardless of the form in which they are used, in the form of whole cells, purified enzymes, or their combination, could greatly facilitate the industrial biomanufacturing of numerous biocommodities [28,41].

Supplementary Materials

The following supporting information can be found at: https://www.sciepublish.com/article/pii/611. Figure S1. SDS-PAGE analysis of XI. Lane M, protein marker; Lane T, total proteins of *E. coli*/ pET20b-XI; Lane S, supernatant of *E. coli*/ pET20b-XI; Lane H, heat-treated supernatant of *E. coli*/ pET20b-XI.

Author Contributions

Y.-H.P.J.Z. conceived the synthetic pathway. X.L. and Y.-H.P.J.Z. designed the experiments, analyzed the data, and wrote the manuscript. P.H. conducted experiments, X.L. performed the experiments. All authors read and approved the manuscript.

Ethical Statement

This article does not contain any studies with human participants or animals performed by any of the authors.

Informed Consent Statement

Not applicable.

Data Availability Statement

The datasets generated during and/or analyzed during the current study are available from the corresponding author on reasonable request.

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Declaration of Competing Interest

The authors declare that they have no conflict of interest.

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